

# **Membranes and membrane technologies. History. Practical aspects.**

# SCIENCE PROGRESS LAST CENTURIES

## Max Karl Ernst Ludwig Planck



1858-1937

- A great scientific idea is seldom introduced by the gradual persuasion and conversion of its opponents. In reality, what happens is that the opponents are gradually passing away. Only the growing generation uses new ideas.
- It means, the period of introducing new ideas is **40-50 years**, i.e. activity of scientists. It is the same period from one scientific revolution to other.

## SCIENCE PROGRESS NOW

The period from one scientific revolution to other is about **5 years** and even less.

**Why?**

- Business and human needs;
- Social elevators, blurring boundaries between classes;
- Internet, digitalization of science.

# Third millennium. Acceleration of scientific progress

## Other political, economical and social reasons

### Reasons caused by destruction

- 
- **Military conflicts with the use of modern weapons;**
- **Elimination of the consequences of military conflicts, man-made disasters, pandemics and natural disasters.**

### Reasons caused by creation

- **Competitions between states and business companies;**
- **Government support;**
- **Positive image of science in society;**
- **Urbanization, raising the educational level of the population;**
- **Creation and development of scientific research centers;**
- **Large amount of scientific and popular science journals;**
- **Internationalization of science, opportunity for scientists to work in different countries. Now the scientists are citizens of the world.**

# Synthetic membranes and membrane separation in the third millennium

- Main scientific revolutions in this field occurred last century, all membrane separation processes are known. Now main efforts are focused on new membrane materials and improvement of known ones. Membrane processes are applied to new objects (fractionality of proteins or aminoacids from mixtures, recovery of RNA, dehydration of biofuel etc.)
- Now biological membranes are in a main focus of attention. They are in the field of investigations of biologists.
- In this lecture, we will consider the **evolution of membrane materials and membrane processes for liquid separations, water decontamination and gas separation**. We will also consider **practical significance** of scientific discoveries in this field.

# PROTOTYPES OF MEMBRANES. FIRST ATTEMPTS OF WATER DECONTAMINATION AND DISINFECTION

## Prehistoric

It is difficult to assume the prototypes of membranes in prehistorical times.



Probably water was purified by means of settling, filtration through sand, finely dispersive rocks or coal from bonfires.

It is only assumption, since we have no proofs .





# PROTOTYPES OF MEMBRANES. FIRST ATTEMPTS OF WATER DECONTAMINATION AND DISINFECTION

## Ancient period



Clay plumbing  
of ancient Egypt



Wells of Ancient Greece



Plumbing of Ancient Rome

**Centralized water treatment** – settling.

**Water treatment in certain households** - filtration through sand, finely dispersive rocks, charcoal or dense textile. Textile can be considered as a **prototype** of modern membranes. This method was already used in the III-II milleniums Before the Common Era.

## Filtration through textile

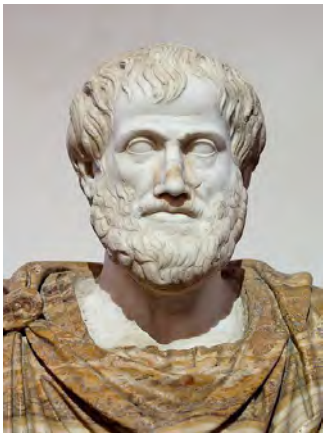


# PROTOTYPES OF MEMBRANES. FIRST ATTEMPTS OF WATER DECONTAMINATION AND DISINFECTION

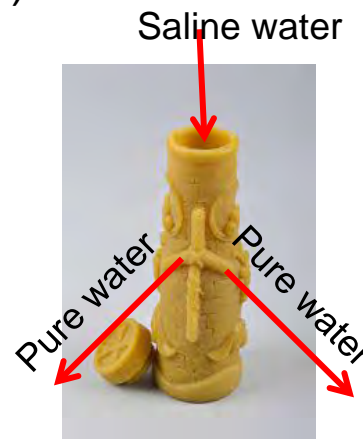
**Filtration through textile allows one to remove only coarse particles. No removal of  $\text{Pb}^{2+}$  ions, which were in water due to lead pipes, was realized. It was the same regarding disinfection.**



**Cyrus** king of Persia (559-530 BCE) supported a use of silverware by warriors to prevent the spread of infections. This disinfection method was available only for reach people. Moreover, a large concentration of silver ions is harmful for the humans. According to the modern standards for drinking water, the maximal allowable concentration of silver ions is 50 ppb ( $0.05 \text{ mg/dm}^3$ ).



**Ἀριστοτέλης, 384-322 BCE**



As a filter for desalination of sea water. Aristotle proposed a wax vessel (Aristotle, Meteorologica). Driving force of water leakage is gravitation. Here the wax matrix is a **prototype** of modern membranes.

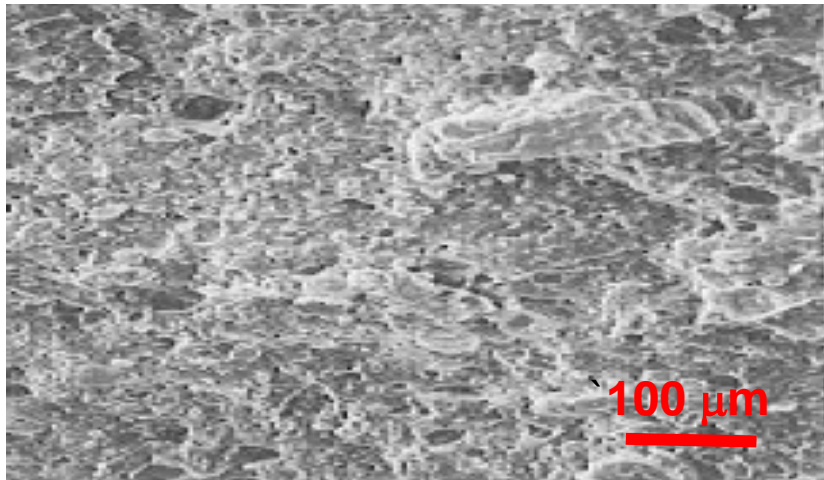
# PROTOTYPES OF MEMBRANES. FIRST ATTEMPTS OF WATER DECONTAMINATION AND DISINFECTION

Was Aristotle right? Is the leakage of deionized water from the wax bottle possible?

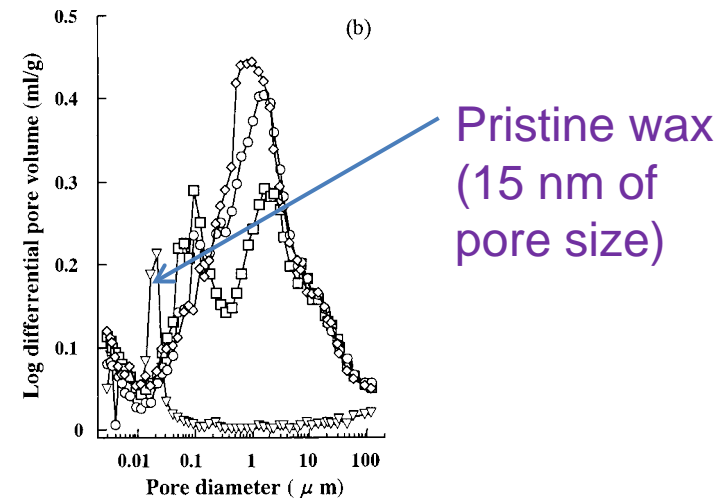
Modern investigations of wax (H.Sato, Y. Miyagawa, T. Okabe et al.

J. Pharmac. Sci. 1997. 86(8): 929-934)

SEM image of wax



Differential pore size distribution

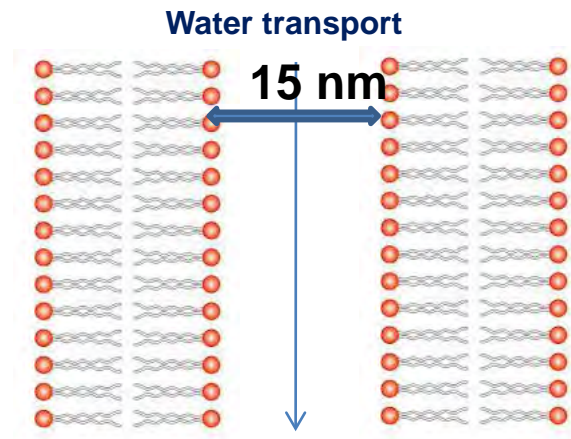




# PROTOTYPES OF MEMBRANES. FIRST ATTEMPTS OF WATER DECONTAMINATION AND DISINFECTION

Was Aristotle right? Is the leakage of deionized water from the wax bottle possible?

Wax consists of different lipids, which involve both hydrophobic and hydrophilic regions. Water is transported through hydrophilic pores.



As follows from pore size distribution, **partial rejection of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{SO}_4^{2-}$  ions.** is possible similarly to ultrafiltration membranes. **Other advantages are disinfection, rejection of colloidal particles.**

**Disadvantages :** water leakage is too slow, singly charged ions remain in water.

# EARLY MODERN ERA. XVIII CENTURY

## Osmosis. “Membrane” term



**Jean Antoine Nollet**  
1700-1770

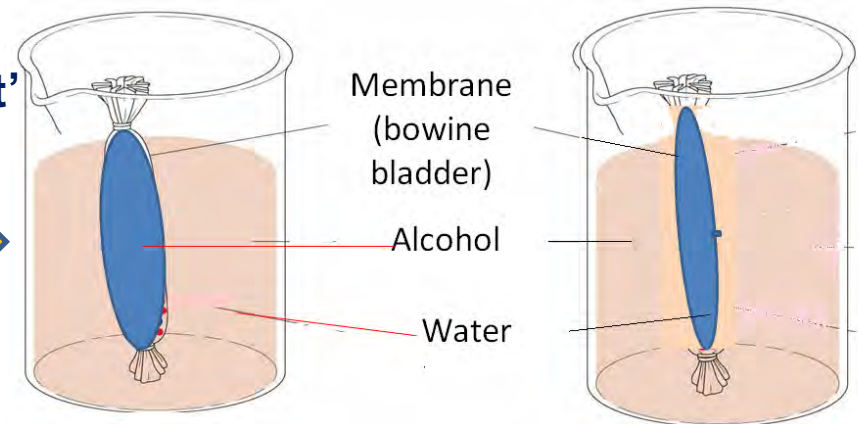
**Osmotic pressure** is the excess hydrostatic pressure from a pure solvent, at which diffusion of solvent stops.

First time Nollet discovered **osmosis** (*ωσμυς* pressure), he introduced a term of “**osmotic pressure**” (1748). Namely Nollet used a “**membrane**” term (lat. *membrana*, i.e. *shell*, *concha*).

**Membrane** is a thin film along perimeter between two spaces, which divides them from each other. Membrane for separation is a semipermeable, it allows penetration of only one kind of species and rejects other ones.

**Osmosis** – transport of liquid through the membrane.

**Scheme of Nollet's experiments**



# EARLY MODERN ERA. XVIII CENTURY

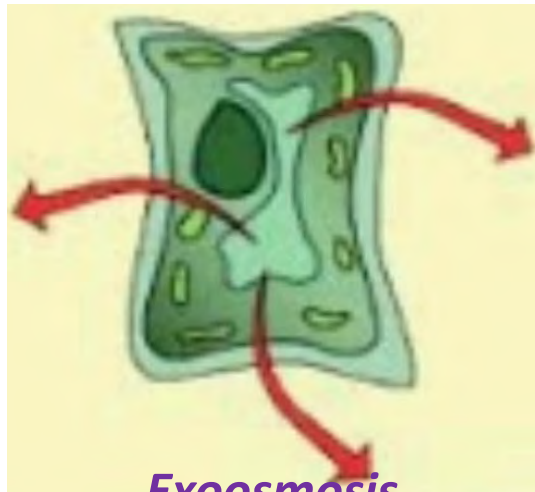
## Rate of osmosis. “Membrane” term



*René Joachim Henri Dutrochet;*  
1776—1847

René Dutrochet established that the rate of diffusion of different liquids through the membrane is proportional to their densities (experiments with ethanol, lavender and olive oil).

He introduced the terms of “exoosmosis” and “endoosmosis”.



*Exoosmosis*



*Plasmolysis*



*Endoosmosis*



*Turgor*

# MODERN ERA. XIX CENTURY

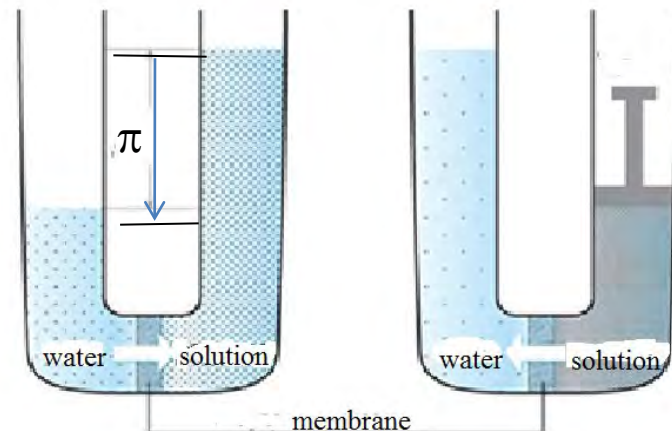
## Osmosis pressure law

The **osmotic pressure of a solution ( $\pi$ )** is equal to the gas pressure that would be produced by the dissolved substance, being in a gaseous state and occupying a volume equal to the volume of the solution.

$$\pi = iCRT$$

$R$  - gas constant,  $i$  - isotonical coefficient associated with the amount of ions produced by 1 molecule.

### Forward osmosis Reverse osmosis



Osmotic pressure depends on the amount of the dissolved substance and independent on its nature and the nature of solvent.



***Jacobus Henricus van't Hoff***

1852 - 1911

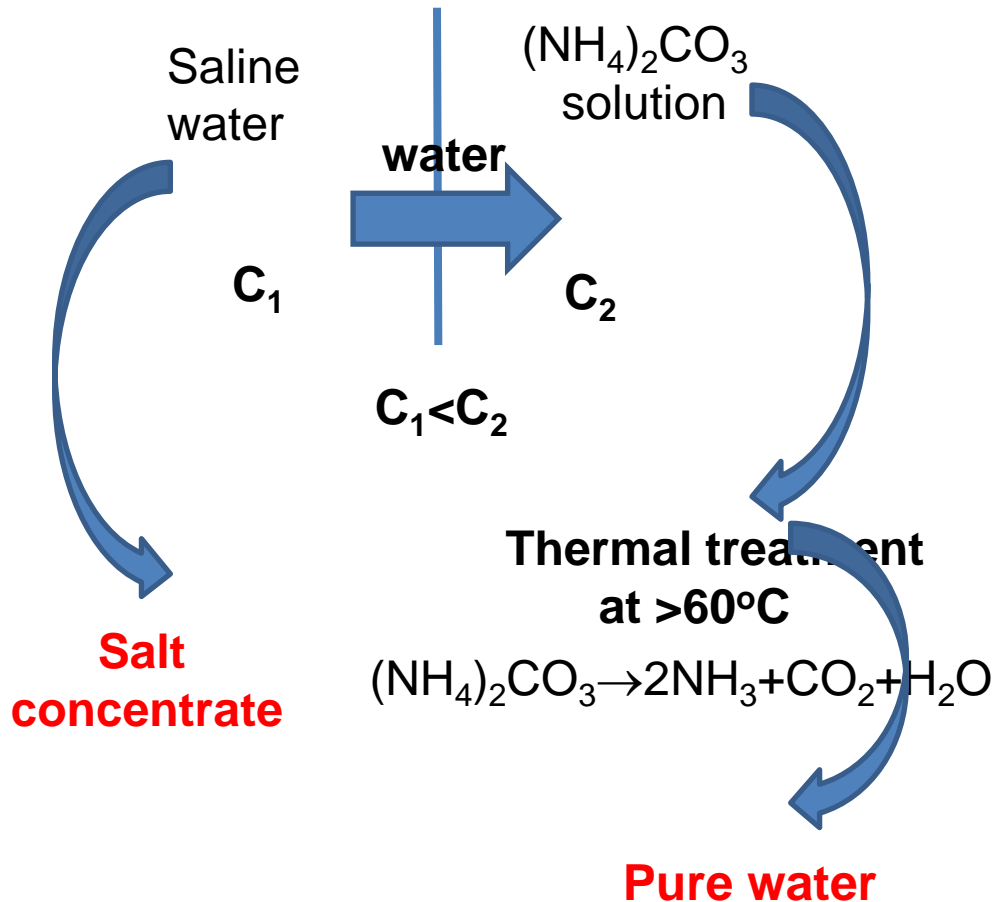
1901. Nobel prize in the field of chemistry for the discovery of laws of chemical thermodynamics and osmosis.

# MODERN ERA. XX CENTURY

## Application of osmosis for water desalination

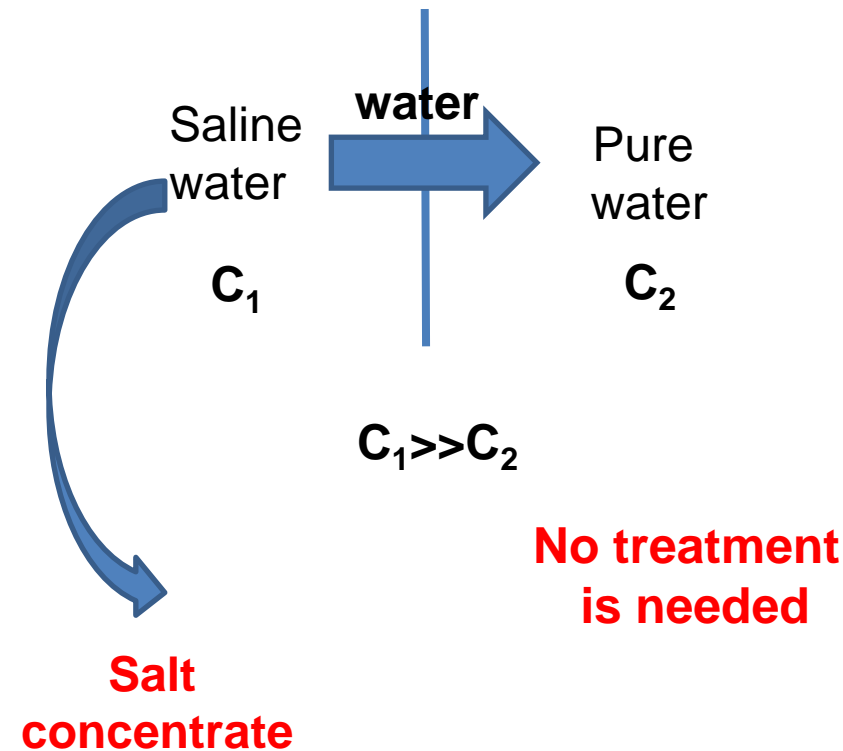
### Forward osmosis

Driven force – osmotic pressure



### Reverse osmosis

Driven force – outer pressure

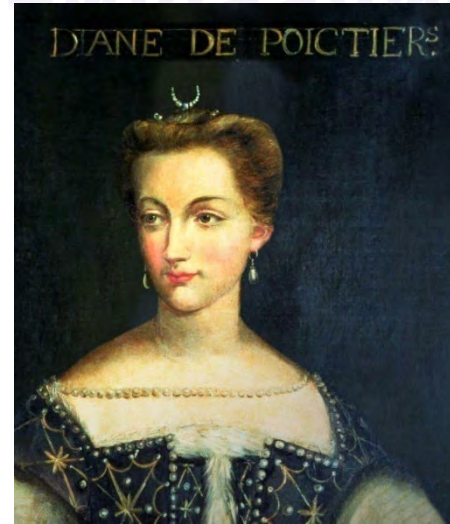




# MIDDLE AGES. RENAISSANCE



**Ambroise Paré (1510-1590)**



**Diane de Poitiers, (1500-1566)**  
**Associated with Henri II Valois**



**Thomas Graham**  
1829 — 1901

Diana looked young until her death. According to one version, doctor Ambroise **Paré** made colloidal gold for her. In order to purify colloidal solution, ceramic or biological membrane (bowine bladder) was used. Namely gold poisoning caused her death. However, **it is impossible to verify this version**, since Diana's grave was destroyed more than 200 years ago during the revolution.

It is suggested officially, that first sol of gold was obtained by **Michael Faraday** in 1857. Later sol was obtained and purified by **Thomas Graham**. Removal of additions was performed using a **parchment membrane**. **Graham is is considered the founder of colloidal chemistry.**

# MODERN ERA

## Membrane method for sol purification

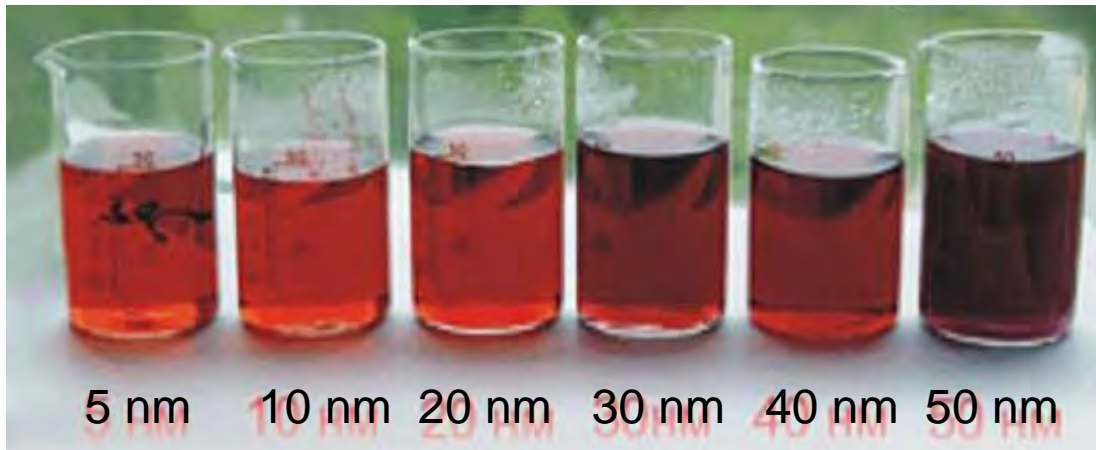
Now sols of precious metal are also in a focus of interest. Sols are currently considered as nanoobjects. Main tasks:

- obtaining nanoparticles of strictly predetermined size (Gaussian narrowing);
- for medical application, a size of nanoparticles must be less than 10 nm (larger nanoparticles are cytotoxic);

**-Deep purification of sol using membranes;**

-- Stabilizing sol.

## Gold nanoparticles. Size effect



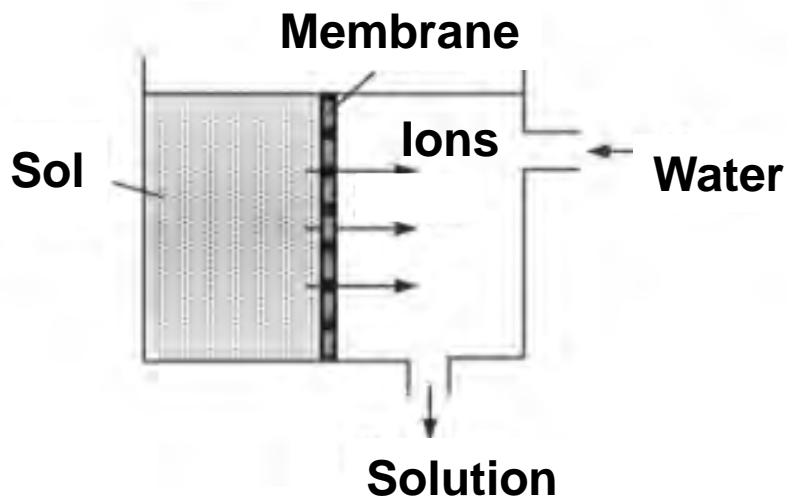
**Increase of concentration gives the same effect**

## Tyndall conus



# MODERN ERA

**Dialysis for sol purification. Driving force is the concentration gradient**



**Dialysis** (from the Greek diálysis — decomposition, separation), removal of impurities of low-molecular substances from colloidal systems using semipermeable membranes. The membranes allow the passage of small molecules and ions, but they reject colloidal particles and macromolecules.

## **Practical application of sols of gold nanoparticles**

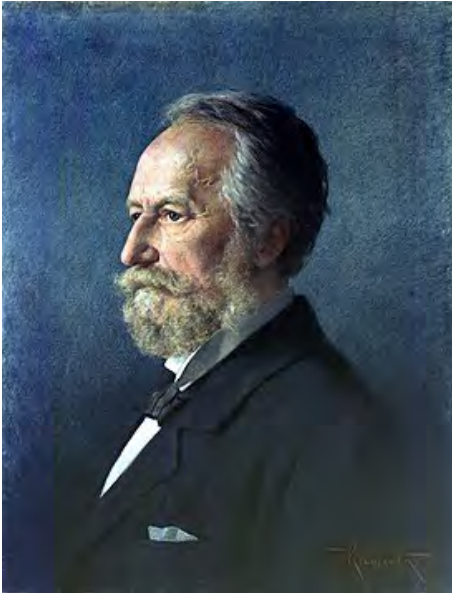
**Medical application:** contraventions of functions of the brain, impaired functions of the circulatory system, depressive states, drug addiction, chronic alcoholism, arthritis, contraventions of function of the endocrine secretion, contraventions of mechanisms of thermoregulation etc.

**Cosmetics:** shampoos, creams, hairsprays.

**Electronics:** spraying on components that cannot withstand the temperature of molten gold. they do not show the temperature of molten gold.

# MODERN ERA

## Development of the theoretical base of dialysis



**Adolf Eugen Fick**

1829 — 1901

**First Fick' law (1885) adapted to the ion transport through membrane:** A flux through the membrane is proportional to the difference in concentrations of solutions on both sides of the membrane and inversely proportional to the membrane thickness.

$$J = D \frac{C_{1,0} - C_{2,0}}{l}$$

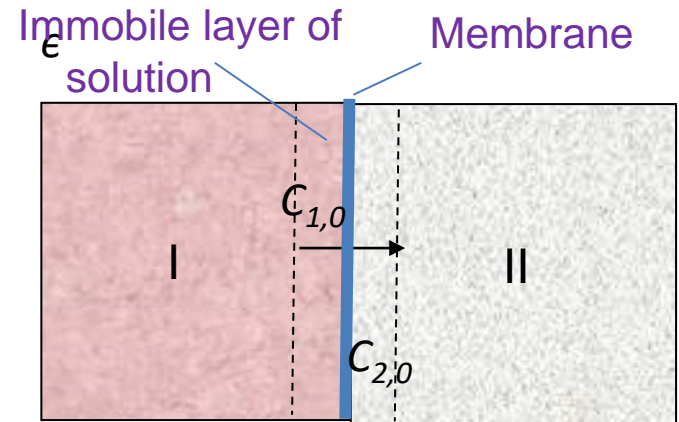
$C_{1,0}$ ,  $C_{2,0}$  – concentration of solutions on both sides of the membranes in a **hydrodynamically immobile layers**.

$D$  – diffusion coefficient of ions in the membrane,

$l$  – membrane thickness.

Dialysis is a too slow process. **The ways to accelerate it:**

- removal of species from the compartment II (combination of dialysis with adsorption),
- decrease of membrane thickness,
- increase of temperature (increase of diffusion coefficient).

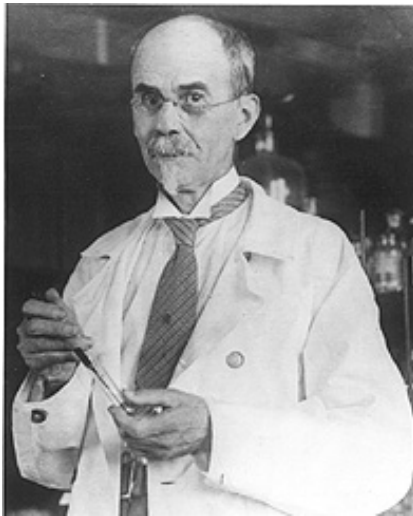




# MODERN ERA

## Practical application of dialysis

- **Hemodialysis** (artificial kidney) is the process of removal of waste products and excess liquid from the body. The principle of hemodialysis is the retention of blood components by the membrane, urea passes to the physiological solution, which is on the other side of the membrane.



**John Jacob Abel**  
1857-1938

1914. John Jacob Abel developed the first hemodialysis apparatus (*dogs were used for the experiments*).

1924– hemodialysis was used in Germany to purify human blood.

## Modern hemodialysis apparatus

### Problems:

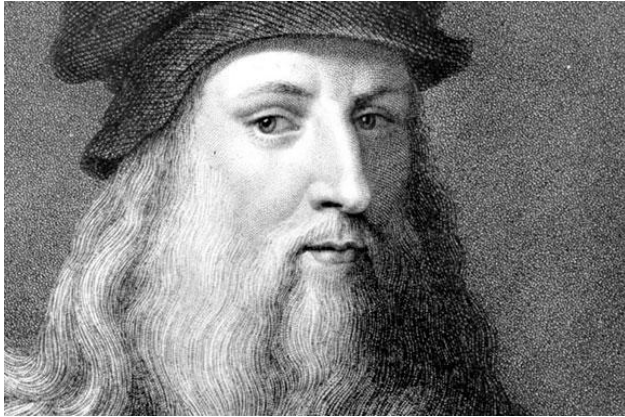
1. *Tromb formation after the contact of blood with membrane.*
2. *To prevent tromb formation, membranes are modified with heparin, which often causes allergic reaction.*
3. *Membranes are permeable towards some blood components,*





# MIDDLE AGE. RENAISSANCE

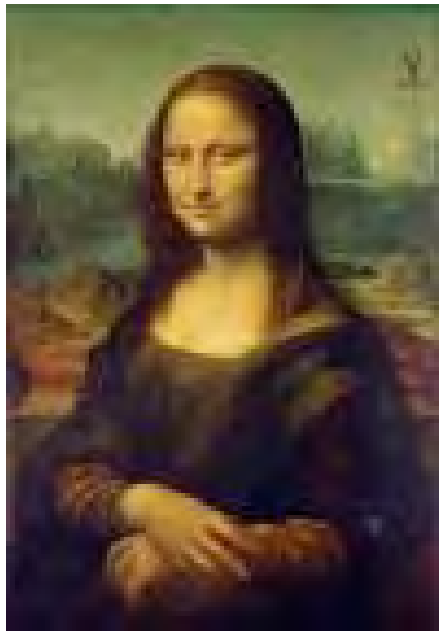
## Development of the theoretical base of membrane processes



***Leonardo da Vinci***  
**1452-1519**

Leonardo da Vinci is a founder of hydrodynamics laws of which determine mass transport in membranes. He suggested an inversely proportional dependence of the rate of water flow ( $u$ ) on the area of the cross-section of a pipe ( $A$ ). In fact, it is a law of flow continuity.

However, Leonardo's authority is contested due to incomprehensible formulation.



***La Gioconda***

Now **Benedetto Castelli** is considered as an author of the law of flow continuity. He was a student of Galileo Galilei.



**Benedetto Castelli**  
**(1577-1644)**

# MIDDLE AGE. RENAISSANCE

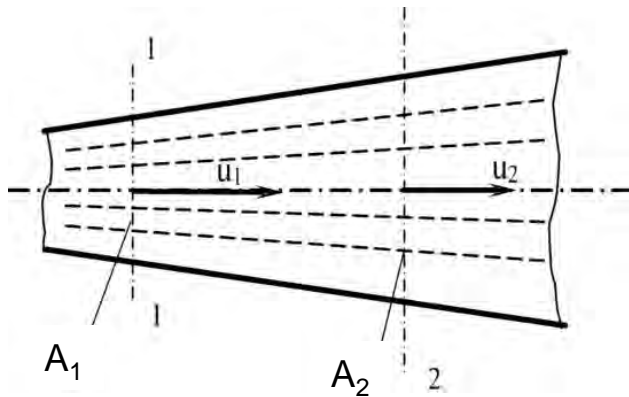
## Development of the theoretical base of membrane processes

The law of the flow continuity is a special case of the law of mass conservation,

### Its simplest formulation for hydrodynamics

The amount of substance passing per unit of time through section 1, e. e. flux  $J_1$  is equal to the amount of substance through section 2, i.e. flux  $J_2$ .

This law is important for asymmetric filtration membranes, which usually consist of macroporous support and active layer containing smaller pores. The fluxes through the cross-sections of different regions are equal. It means, the amounts of substance at the “inlet” and “outlet” of the membrane are equal.

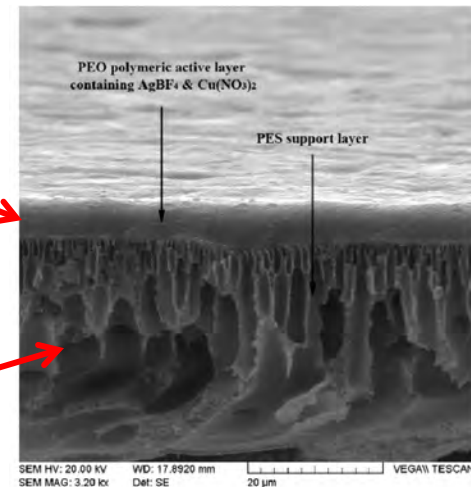


$$J_1 = J_2$$

$$\frac{u_1}{A_1} = \frac{u_2}{A_2}$$

Active layer

Macroporous support



The fluxes through each region of asymmetric membranes are similar.

# EARLY MODERN

## Development of the theoretical base of membrane processes

The law of energy conservation during stationary flow of an incompressible ideal fluid.



**Daniel Bernoulli**  
1700-1782

### Vertical flow

$$\frac{\rho u^2}{2} + \rho gh + p = \text{const}$$

I                      II           III

### Horizontal flow

$$\frac{\rho u^2}{2} + p = \text{const}$$

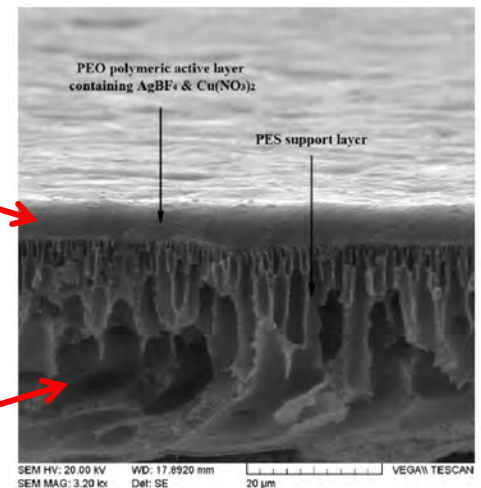
I                      III

Term I – dynamic pressure, term II – hydrostatic pressure, term III – static pressure (pressure of molecules on pipe wall),  $\rho$  - fluid density,  $h$  – pipe height,  $g$  – acceleration of free fall.

For asymmetric membranes, the pressure in each region is a constant value.

Active layer

Macroporous support



# EARLY MODERN

## Development of the theoretical base of membrane processes



**Isaac Newton**  
1642-1727



**Gottfried Wilhelm Leibniz**  
1646-1716

Basics of differential and integral calculus were developed. For instance, the expression for flux can be adapted to barometric filtration:

$$J = \frac{dV}{dt} \frac{1}{A}$$

$V$  – cumulative permeate volume.

Representation form for differential like  $dV/dt$  has been proposed by **Leibniz**.

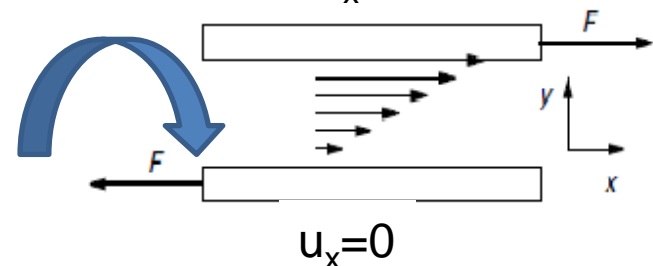
## Newton' law of viscous friction for the moving layers of liquid

The force of viscous friction of moving layers of liquid ( $F$ ), which are in contact with each other, is proportional to the velocity gradient. The proportionality factor is called “dynamic viscosity coefficient” ( $\mu$ ).

$$F = \mu \frac{du}{dy} A$$

Viscosity of liquids determines mass transport through membranes.

**Profile of velocities**  $u_x = u$



# MODERN ERA. XIX CENTURY

## Main law for the filtration through porous media



**Henry Darcy**  
**1803-1858**

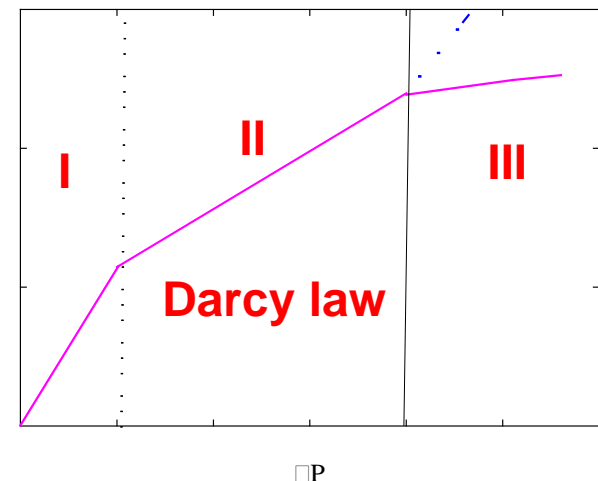
The law was obtained based on experimental data for rocks.

$$J = \frac{\Delta P}{\mu R}$$

$R$  is the hydrodynamical resistance. The Darcy law is applicable for the filtration membranes.

II – region of Darcy law  
I and III – deviations from Darcy law

Permeate flux through the filtration membrane vs pressure



**Region of low pressure** – penetration of the aqueous solution into hydrophobic pores.

**Region of high pressure, slowdown of filtration** – reversible membrane compression, transition from laminar flow to turbulent flow, growing of osmotic pressure, which acts in reversible direction of outer pressure.

**Region of high pressure, acceleration of filtration** – stretching of pores, leakage of modifier.

The behavior of one or other membrane strongly depends on its material.

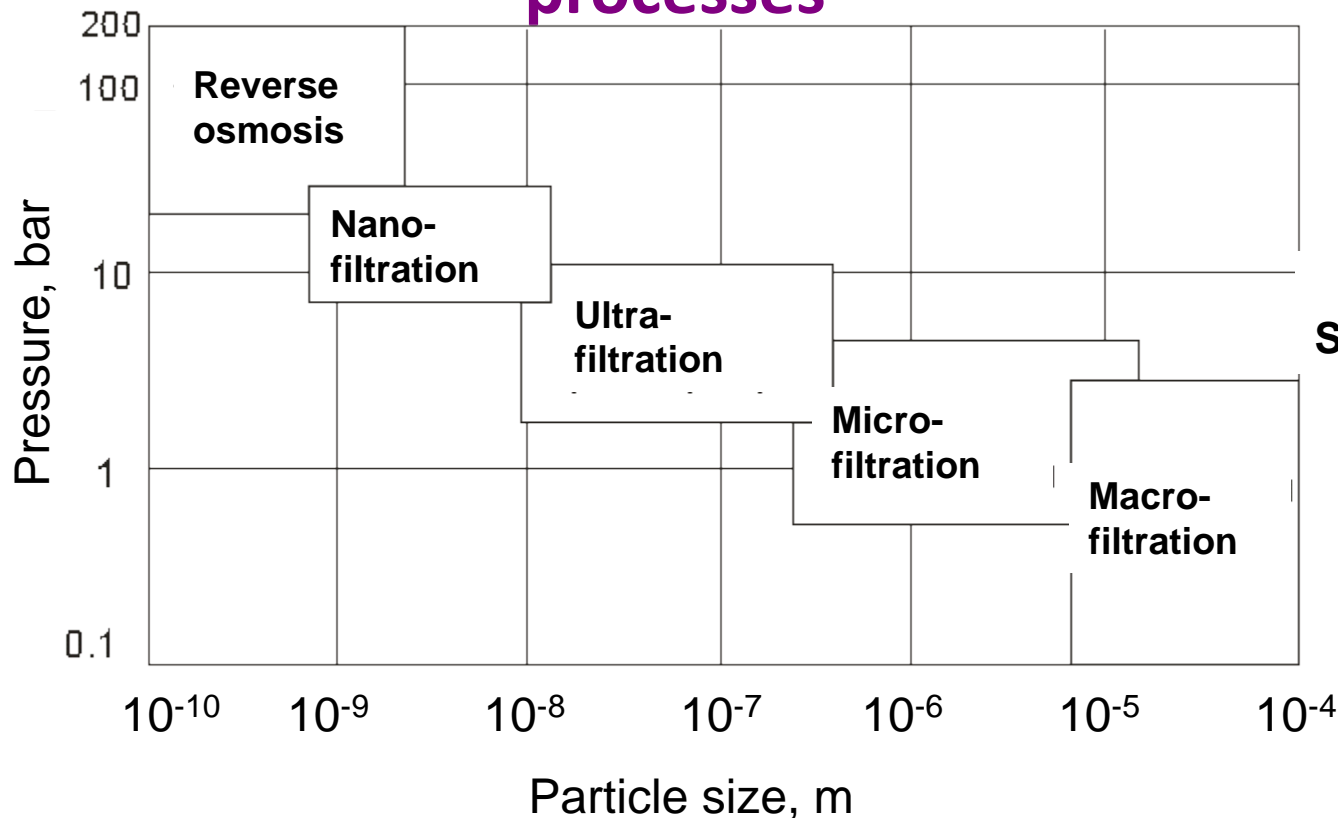


# MODERN ERA. XX CENTURY

## Baromembrane separation

Despite considerable theoretical basis and experimental results, filtration processes were invented and commercialized, when suitable membrane materials were obtained.

### Classification of baromembrane processes



### Thickness of active layer

**Macrofiltration**

No active layer

**Microfiltration**

10-150  $\mu\text{m}$

Some membranes -0.1  $\mu\text{m}$

**Ultra-, nanofiltration, reverse osmosis**

0,1-10  $\mu\text{m}$

# APPLICATION OF BAROMEMBRANE PROCESSES TO DIFFERENT SPECIES

Species	Size, nm	Method
Yeast, mushrooms	1000-10000	Macro-, microfiltration
Bacteria	300-10000	Macro-, micro-, ultrafiltration
Oil emulsions	100-10000	Macro-, micro-, ultrafiltration
Solid colloidal particles	100-1000	Micro-, ultrafiltration
Viruses	30-300	Micro-, ultrafiltration
Proteins, polysaccharides	2-10	Ultra-, nanofiltration
Enzymes	2-5	Ultra-, nanofiltration
Antibiotics	0.6-1.2	Nanofiltration, reverse osmosis
Organic molecules	0.3-0.8	Reverse osmosis
Inorganic ions	0.2-0.4	Reverse osmosis
Water	0.18	

# Macrofiltration

**Water jet pump**



**Schott filter**



**Paper filter or Shott filter  
size of rejected particles up to 1.5  $\mu\text{m}$**

# MODERN ERA. XX CENTURY

## Ultrafiltration

**Background:** Filtration of proteins and gum through animal membranes

*Schmidt: Ann. Phys. Chem. 99, 337 (1856)*

Filtration of blood plasma *in vivo*

*Sanarelli: Cent. Bakt. Parasitenk., 467.(1891)*

Filtration of enzymes

*Levy: J. Infectious Diseases 2,1 (1905).*



**Heinrich Jakob Bechhold**  
1866-1937

### 1907. Development of ultrafiltration method.

**1 stage.** – Modifying filter paper with cellulose acetate. A series of membranes with graded porosity was obtained by H.J. Bechhold.

**2 stage.** - The technique for the determination of pore size (bubble method) has been proposed.

**3 stage.** -Considered a role of adsorption in filtration processes.

### 1926. Development of hermetic filter (membrane cartridge)

# MODERN ERA. XX CENTURY

## MICROFILTRATION



***Richard Adolf Zsigmondy***  
**1855-1929**

1925 p. - Nobel Prize in Chemistry for establishing the heterogeneous nature of colloidal solutions and developing methods for their research (immersion microscopy).

**1918. Development of microfiltration method using nitrocellulose and cellulose-ester membranes**

Zsigmondy R., Bachmann W.: 1918, „Ueber neue Filter,“ Z. Anorg. Allgem. Chem. 103: 119–128..

**2021. US patent protects the invention.**

The **Membran-Filtergesellschaft Sartorius Werke** company has been found, the company produces microfiltration membranes. This company is working now, its branches are in many countries.



# MODERN ERA. XX CENTURY

## REVERSE OSMOSIS



**Charles E. Reid**  
**1917-2000**

**1953.** Main principles of reverse osmosis were formulated. It was shown that in order to obtain pure water from salt solutions, it is necessary to apply pressure to the system that exceeds the osmotic pressure.

*C. E. Reid, E. J. Breto. Water and Ion Flow Across Cellulosic Membranes. J, Appl. Polym, Sci. 1959. 1(2): 133-143.*

1960. Rapid development of reverse osmosis, since special membranes have been developed by Loeb and Surirajan.

**Loeb S., Sourirajan S.** *In:* Saline Water Conversion—II, ACS Publications. 1963. V. 28. P. 117-132.

Membranes were prepared based on cellophane and cellulose acetate, which were modified by silicone. Other commercial materials were also used. The membrane with the best characteristics produced 200-450 dm<sup>3</sup> m<sup>-2</sup> of permeate per day under a pressure of 100-140 bar. A 5-.25% NaCl solution was desalinated. The final NaCl content was 0.05%. Very high pressure is caused by non-porous active layer.

# MODERN ERA. XX CENTURY

## NANOFILTRATION

Two ways **to decrease pressure** for reverse osmosis processes.

- To **reduce a thickness of the active layer** (the value of minimal thickness is limited);
- To **allow nanopores** (1-2 nm or a little bit larger), where double electric layers are overlapped.

1988. – Peter Eriksson (USA). *P. Eriksson. Nanofiltration extends the range of membrane filtration. Environ. Progr. 1988. 7(1): 58-62.*



**Andria Yaroshchuk**

1970-1990. The theory was developed particularly in the Institute of Colloidal Chemistry and Chemistry of Water of the National Academy of Science of Ukraine.

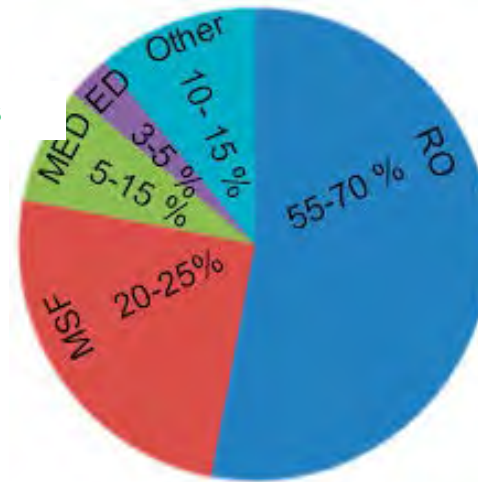
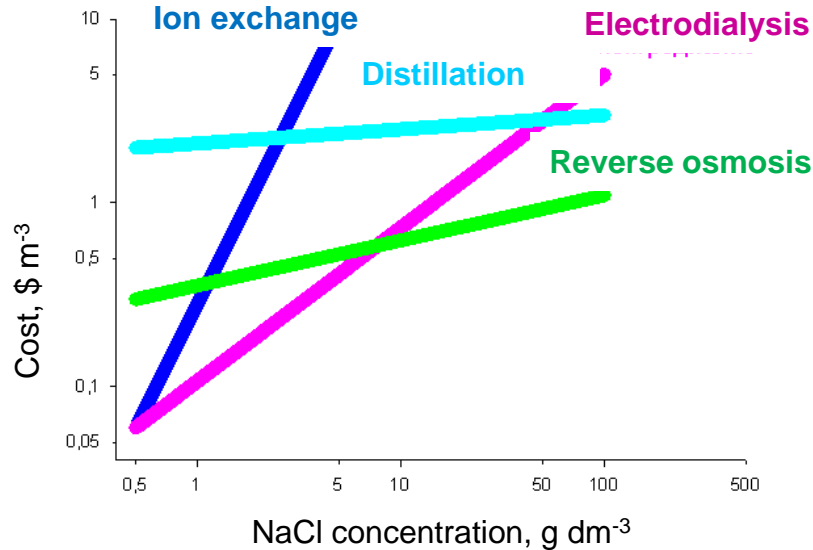
[A Yaroshchuk, E Staude. Charged membranes for low pressure reverse osmosis properties and applications. Desalination. 1992 86\(2\): 115-133.](#)

Nanofiltration allows us to remove hardness ions and heavy metals, arsenic compounds, phosphates, pesticides, and polysaccharides from liquids.

**Problems:** purification strongly depends on the composition of concentrate. Rejection ability of membranes is affected by adsorption.

# Economical efficiency of different methods of water desalination

## Contribution of various methods to global freshwater production



ED- electrodialysis,  
RO – reverse osmosis,  
MED –multiple-effect  
distillation,  
MSF – multi-stage flash  
distillation

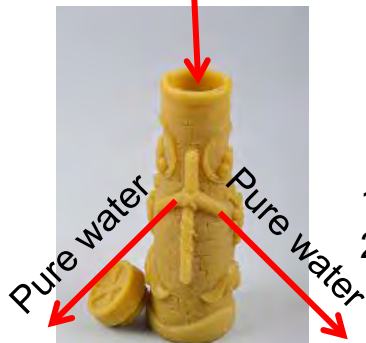
## WATER DESALINATION: FROM ARISTOTEL

### Ancient period

Saline water

Plant of sea water  
desalination,  
опріснення води,  
Ashkelon, Israel

127 millions m<sup>3</sup>per year,  
20 % of the country needs



### Now



# **MEMBRANES FOR GAS SEPARATION**

# MODERN ERA. XIX CENTURY

## Diffusion through membranes. Different behavior of gases

The balloons made of caoutchouc, which were filled with different gases, decreased their volume with different rate depending on the gas. Hydrogen left balloon faster than air, but the fastest gas was  $\text{CO}_2$ .

Mitchell noted that  $\text{CO}_2$  was adsorbed by the caoutchouc film. He suggested that pores of the film provide gas leakage.

***Mitchell, J. K., On the Penetrativeness of Fluids, J. Roy. Inst., 4, 101-118; 5, 307-321 1831.***



***John Kearsley Mitchell***  
**1793-1858**





# MODERN ERA. XIX CENTURY

## Diffusion through membranes. Different behavior of gases



*Thomas Graham*

1829 — 1901

Thomas Graham used an apparatus to study the diffusion of gases .

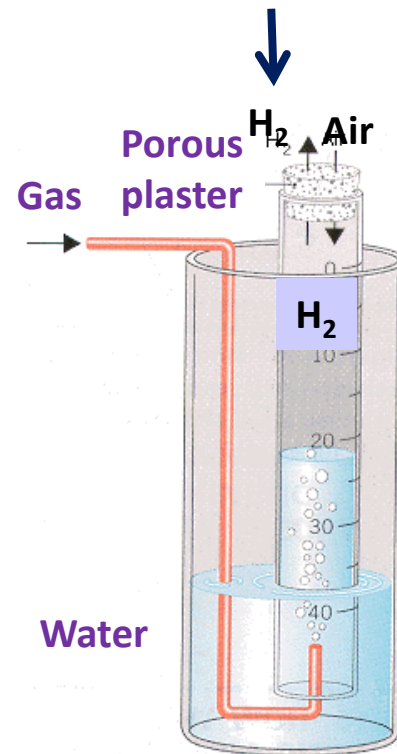
This apparatus consists of a glass tube sealed at one end with porous plaster.

When the tube is filled with  $H_2$  gas, the level of water in the tube slowly rises.

This is due to the leakage of  $H_2$  from the tube through the porous plaster. Hydrogen left the tube more rapidly than air can enter instead of it.

The rate of the change of the water level was studied. Based on these data, Graham estimated the rate, at which different gases mixed with air.

Gas ( $H_2$ ) escape through porous material



# MODERN ERA. XIX CENTURY

## Illuminating gas – typical object for investigations

- **Illuminating gas** was also an object of investigations by Graham. It is obtained by pyrolysis of coal or oil. Illuminating gas consists of  $H_2$  (50 %),  $CH_4$  (34 %),  $CO$  (8 %) and other combustible gases. It was developed by in the first half of the XIXth century by *Friedrich Christian Accum* (1760-1838). Illuminating gas was used for lighting in gas lamps and as fuel in XIXth and in the first half of the XIXth century.

- Illuminating gas in **psychology** – “**gaslighting**”. This term is derived from the American movie “Gaslight” (1944).



Purification of gas lamp in Westminster, London, 2011



Charles Boyer  
as Gregory Anton/Sergis Bauer  
Ingrid Bergman  
as Paula Alquist Anton

# MODERN ERA. XIX CENTURY

## Diffusion of gases through membranes

- Graham also studied diffusion of illuminating gas through membranes (natural caoutchouc, guttapercha, platinum, palladium). Probably metallic particles were deposited chemically to natural or ceramic membranes (???)
- Faster diffusion of  $\text{CO}_2$  and  $\text{H}_2$  comparing other gases was found.
- Adsorption of hydrogen by Pt and Pd was suggested.
- Quantitative characteristics of membrane permeability with respect to oxygen, air,  $\text{CO}_2$ , CO, methane, etc. were determined. The rate of gas penetration is determined by pressure.
- Effusion was investigated. Effusion is a slow escape of gas through porous materials, molecules move in pores without collisions with each other. This is possible, when the pore diameter is much smaller than the length of the free path of the molecules. This distinguishes effusion from diffusion, when many molecules can penetrate through pores simultaneously.

# MODERN ERA. XIX CENTURY

## Effusion of gases through membranes. Graham's law

**Graham's law** states that the rate of diffusion or of effusion of a gas ( $Q$ ) is inversely proportional to the square root of its density ( $\rho$ ) or molecular weight ( $M$ ) at constant temperature and pressure.

$$Q \times \sqrt{\rho} = \text{const}$$

The **constant** is approximately **similar** for all gases

For two different gases:

$$\frac{Q_1}{Q_2} = \sqrt{\frac{M_2}{M_1}}$$



**It means, the effusion rate is higher for lighter gas.**

For instance, a balloon loses helium faster than air.

Further the theory of gas leakage through small pores was developed by Knudsen.

# MODERN ERA. XIX CENTURY

## Penetration of gases through membranes. Knudsen model



Knudsen established that in pores with a pore diameter smaller than the length of the free path, the permeability cannot be described not only by the laws of viscous flow, but also by the laws of diffusion.

In order to describe permeability, the analogy with friction was used.

Now it is generally accepted that the Knudsen model is valid only in mesopores ( $2 \text{ nm} < d < 50 \text{ nm}$ ). Though it is difficult to say about free path.

In macropores ( $d > 50 \text{ nm}$ ), laws of molecular diffusion are valid. In micropores ( $d < 2 \text{ nm}$ ), molecules interact with pore walls.

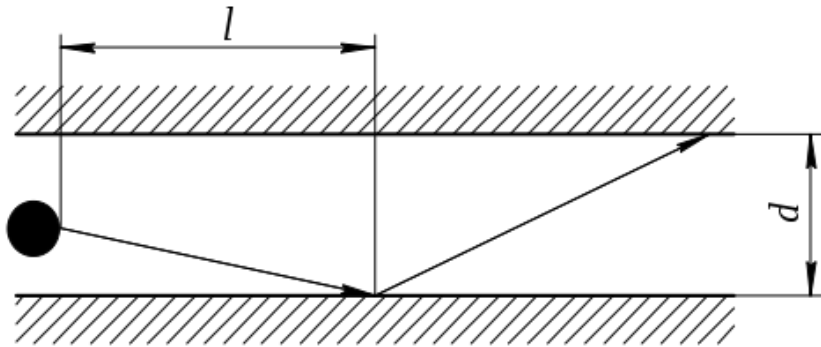
***Martin Hans Christian Knudsen***

**1871-1949**



# MODERN ERA. XIX CENTURY

## Penetration of gases through membranes. Knudsen model



The transition from ordinary diffusion in gases to Knudsen diffusion is characterized by a dimensionless parameter - Knudsen criterion ( $Kn$ ):

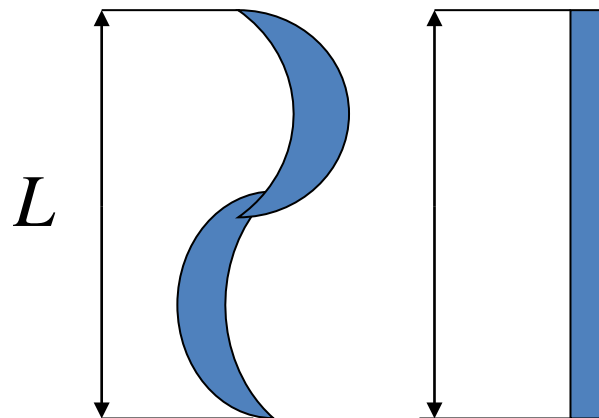
$$Kn = \frac{l}{d}$$

$l$  – length of free pass,  
 $d$  – pore diameter

$l = 68$  nm at 1 bar for molecules of  $O_2$ ,  $N_2$  and  $CO_2$ .

$Kn \gg 1$  - the probability of collisions of gas molecules with pore walls significantly exceeds the probability of collisions of molecules with each other.

## Rate of gas through membrane ( $Q$ )



$$Q = \frac{\Delta P d^3}{6LP} \sqrt{\frac{2\pi RT}{M}}$$

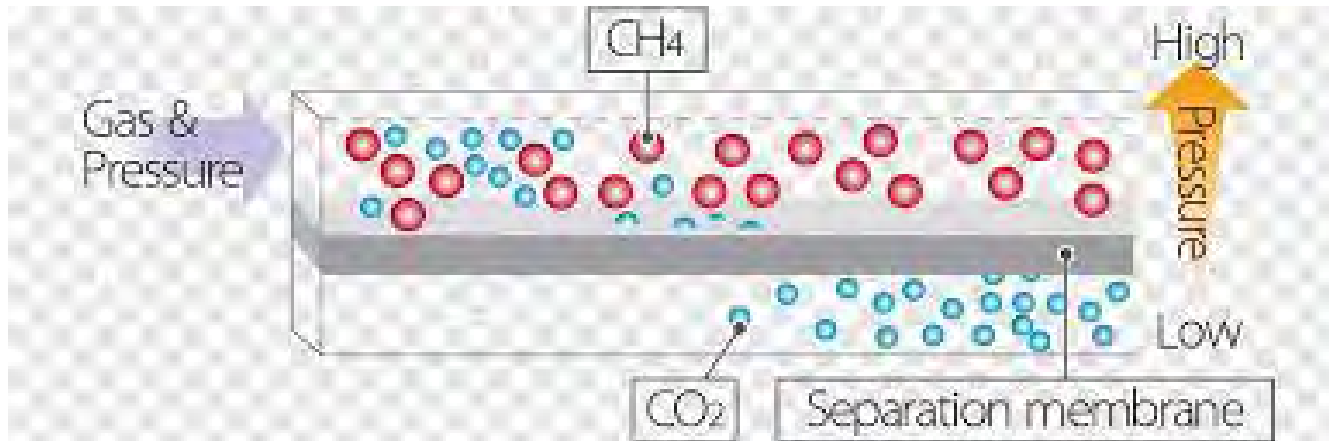
$\Delta P$  – difference of pressure between pore ends,  
 $P$  - average pressure in a pore,  
 $L$  – pore length

The  $LP$  parameter characterizes the tortuosity and narrowing-expansion of pores. The smaller this value, the higher rate of gas.

# MODERN ERA. XX AND XXI CENTURIES

## Practical application of Graham' and Knudsen' works

### Development of membrane gas separation.



**Driven force is the pressure gradient**

**The first membrane produced in industrial scale was made of poly(vinyltrimethyl)silane. The membrane was made in the middle of 1970 in the USSR. A thickness of dense layer was 0.2-0.4  $\mu\text{m}$ , the overall thickness of the membrane was 100  $\mu\text{m}$ .**

**Now the main producers of the membranes for gas separation are DuPont and Monsanto companies (USA).**

# MODERN ERA. XX AND XXI CENTURIES

## Practical application of Graham' and Knudsen' works

### Military needs.

- Estimation of air leakage form spaceships and submarines. In order to remove  $\text{CO}_2$  from air, special devices containing silicon membranes are used.



# MODERN ERA. XX AND XXI CENTURIES

## Practical application of Graham' and Knudsen' works

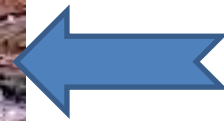
### Military needs

**Atmolysis** is the separation of a mixture of gases of different densities by multiple passing them through membranes.

1942. The multi-stage device for **the separation of uranium isotopes** was built in Oak Ridge (USA), Natural uranium is an isotopic mixture with 0.7%  $^{235}\text{U}$  and 99.3%  $^{238}\text{U}$ . Uranium is transformed into volatile  $\text{UF}_6$ , which is passed through the membranes. The diffusion rate of the  $^{235}\text{U}$  isotope is higher only in 1.004 times comparing with  $^{238}\text{U}$ . In order to obtain enriched uranium, membrane separation has to be repeated thousands times.



Gas centrifuge instead of membrane separation was used in the USSR.



*The plant for uranium enrichment in Oak Ridge.*

# MODERN ERA. XX AND XXI CENTURIES

## Practical application of Graham' and Knudsen' works

### Oxygen concentrator



Membrane device is used for chirurgia. Oxygen diffuses through the silicone membrane into the blood. Oxygen dosing prevents protein denaturation and gas bubbles.

**Especially the oxygen concentrator was important during COVID pandemic.**

It is possible to increase  $O_2$  concentration in air up to **33 %** (I stage) and **91%** (V stage). Graham obtained **46%**.

It is possible to increase  $O_2$  concentration in air up to **33 %** (I stage) and **91%** (V stage) ). **Graham** obtained **46%**.



# CONCLUSIONS

## Synthetic membranes and membrane separation in the third millennium

- Main scientific revolutions in this field occurred last century, all membrane separation processes are known. Now main efforts are focused on new membrane materials and improvement of known ones. Membrane processes are applied to new objects (fractionality of proteins or aminoacids from mixtures, recovery of RNA, dehydration of biofuel etc.)